**UHMWPE-Layered Silicate Nanocomposites by in situ Polymerization with Tris(pyrazolyl)borate Titanium/Clay Catalyst**

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Nanocomposites of polyethylene-MMT were prepared through the methodology of in situ polymerization using Tp[^6−]TiCl₃ (I) intercalated into the gallery of Cloisite® 30B (C30B) using methylaluminoxane (MAO) as activator. From the powder X-ray diffraction (XRD) analysis it was observed that the basal spacing of the activated organoclay changes from 1.85 nm (2θ = 4.8) to 2.18 nm (2θ = 4.0) indicating the occurrence of intercalation of the catalytic system 1/C30B/MAO into the ethylene polymerization due to different reaction conditions. The morphology of the exfoliated morphology of the PE-MMT nanocomposite was further examined and confirmed by X-ray diffraction (XRD) and transmission electron microscopy (TEM) analysis. The presence of exfoliated clay (5% by weight) in the PE matrix confers better mechanical properties (flexural modulus and storage modulus) when compared with those displayed by the neat PE produced using exclusively 1.

**Keywords:** clay, UHMWPE, nanocomposites, titanium catalyst

**Introduction**

In recent years, polymer-clay nanocomposites have attracted much academic and industrial interest because of the anticipated improvements in mechanical properties, stiffness, thermal stability, chemical resistance, high barrier properties, flame retardancy, etc. when the aluminosilicate platelets of clays like montmorillonite are well exfoliated into polymers. Inorganic layers with polymers, template synthesis of layered crystals in the polymer solution, melting intercalation, and direct ion exchange of polyelectrolyte with hosts. More recently, special attention has been devoted to in situ intercalative polymerization methodology which is frequently also referred to as “polymerization filling”. In this process, the monomer together with the polymerization initiator or catalyst is intercalated within the silicate layers and the polymerization is initiated either thermally or chemically. In contrast to highly viscous polymer melts, the polymerization reaction media have much smaller viscosity and enable easy dispersion of nanoparticles, provided that the compatibilities of media

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and nanoparticles are matched. Moreover, polymerization filling process can produce nanocomposites with much higher nanofiller content. This strategy has been utilized to produce a variety of economically important polymer-clay nanocomposites based on poly(methyl methacrylate), poly(lactic acid), polyurethanes, poly(ε-caprolactone), and polystyrene. Furthermore, this approach has been extremely useful to produce well-exfoliated nanocomposites based on apolar polyolefins in spite of their hydrophobic properties that lack suitable interactions with the polar aluminosilicate surface of the clay. In this case, the vast majority of these studies are concerned to polypropylene, linear low-density polyethylene, and high-density polyethylene. On the other hand, just one example of ultra high molecular weight polyethylene (UHMWPE)-layered silicate is described in the literature using polymerization filling technique. For instance, Jérôme and co-workers reported the production of UHMWPE nanocomposites by in situ intercalarization polymerization process using a titanium catalyst [Me₃Si(Me₅Cp) (N'Bu)]TiMe₂. Herein, we report the synthesis and characterization of intergallery-anchored Tp⁶⁺TiCl₃ (Tp⁶⁺= HB(3-mesitylpyrazolyl)(5-mesitylpyrazolyl)⁺) into an organophilically modified montmorillonite clay (Cloisite® 30B), by methyl, tallow, bis-2-hydroxyethyl quaternary ammonium chloride (MT₄EtOH), and its application in the production of UHMWPE-layered silicate nanocomposites.

**Experimental**

**Materials**

All manipulations were carried out under Ar atmosphere using standard Schlenk tube techniques. Tp⁶⁺TiCl₃ was synthesized following procedures described in the literature. Cloisite® 30B (Southern Clay Products) was dried under vacuum (P < 10⁻¹ mbar) for 8 hours at 150 °C. Ethylene (polymer grade), provided by White Martins, and argon were deoxygenated and dried through column of BTS (BASF) and molecular sieve (3A) activated prior to use. MAO (Witco, 5.21 wt.% toluene solution which contains ca. 20 wt.% TMA, trimethylaluminum) was used as received. Toluene and hexane were refluxed and distilled over sodium diphenylketyl complex prior to use.

**Intercalation procedure of Tp⁶⁺TiCl₃ into the activated-Cloisite® 30B**

A toluene solution of Tp⁶⁺TiCl₃ (1) (0.021 g, 30 µmol) was canulla-transferred into predried Cloisite® 30B (1.0 g) toluene slurry (20 mL). The reaction mixture was stirred at ambient temperature for 24 h. The slurry was then filtered through a fritted disk. The resulting solid was washed several times (ca. 5 × 10 mL) with toluene at 50 °C, and dried under vacuum for 24 h. The resulting solid was named 1/C30B.

**Polymerization procedures**

All polymerization reactions were performed in Fisher-Porter reactors (0.1 L or 4 L) equipped with mechanical stirrer. Under ethylene atmosphere, the proper amounts of solvent (toluene or hexane) and MAO were introduced sequentially. After complete thermal equilibration, the slurry solution containing 1 or 1/C30B was added with stirring. The total pressure was kept constant by a continuous feed of ethylene. The polymerization runs were stopped by introducing acidic ethanol. The polymers were washed with acidic ethanol, then ethanol and water, and dried in a vacuum oven at 60 °C for 12 h.

**Intercalated Ti catalyst and PE-nanocomposite characterization**

An inductively coupled plasma optical emission (ICP-OES) spectrometer from PerkinElmer (Optima™ 2000 DV) was used for Ti measurement in the clay. A Scott spray chamber and a GemCone® nebulizer composed the sample introduction system. Catalyst digestion was done with H₂SO₄ and HNO₃ (H₂SO₄/HNO₃ 3:1) in Teflon® capped vessel. The mixture was heated at 160 °C for 8 h in a heating block (Tecnal, Brazil). Sample and blank were analyzed in duplicate. The intrinsic viscosity of the neat PE and PE-MMT nanocomposite samples were analyzed using in a modified procedure in which the PE was firstly dissolved in decaline (concentrations of 0.02 g dL⁻¹) at 165 °C, filtered through a 0.2 mm filter in order to remove the clay structure and then the PE solution was transferred quickly to a modified Ubelohde viscosimeter at 135 °C. Based on the experimental intrinsic viscosity values [η] it was possible to calculate the viscometric molar mass according to the formula [η] = k(Mₐ)ᵃ, for k = 6.7×10⁻⁴ dL g⁻¹ and α = 0.67. Thermal and crystallization behaviors were determined using Thermal Analysis 2100/TA Instruments. The temperature and energy readings were calibrated with indium and zinc according to ASTM D3417 and D3418. All measurements were carried out in nitrogen atmosphere. The sample was heated to 150 °C, kept at this temperature for 5 min, then cooled and heated at constant rates of 5 °C min⁻¹. Thermogravimetric (TG) was carried out under dried air with a Thermal
Analysis Instruments Q500 Thermogravimetric Analyzer with a heating rate of 10 °C min\(^{-1}\) from room temperature to 900 °C. The percentage of residual ashes (filler) was taken as the value reported at 600 °C. Dynamic Mechanical Thermal Analysis (DMTA) was carried out using a TA Instruments 2980 operating in the tensile mode. The sample dimensions were 0.15×7.0×12 mm. Measurements were taken at 1 Hz. The temperature was raised from −150 to 150 °C, at a scanning rate of 2 °C min\(^{-1}\). The flexural moduli of the nanocomposites were evaluated using a Universal Test Machine (INSTRON 4204) according to ASTM D-790. The tensile bars (at 23 °C) of neat and PE-clay were submitted to a deformation force over two supports, the force was applied at the bar central point at selected displacement rate of 13 mm min\(^{-1}\), the sample dimensions were 13x57x19 mm. Heat Deflection Temperature was measured using a CEAST Vicat Auto machine Model P/N 6970.000 according to ASTM D 648. The sample position was edgewise and surface stress was 0.45 or 1.82 MPa. Silicon oil was used to facilitate the heat transfer; the temperature was registered at 0.25 mm deflection. The X-ray diffractograms were obtained with a Siemens D-500 diffractometer. Films were scanned in the reflection mode using an incident X-ray of Cu K\(\alpha\) radiation with wavelength of 1.542 Å at a step size of 0.05° min\(^{-1}\) from 2\(\theta\) = 1° to 10°. The transmission electronic microscopy analysis was carried out using ultra thin cuts obtained from the compressed specimens in a JEOL JEM-120 EXII TEM microscope operating at an accelerating voltage of 80 kV. The cuts were placed on 300 mesh Cu grids.

**Results and Discussion**

The organomodified Cloisite® 30B (C30B) was selected considering the hydroxyl groups attached to the alkylammonium cations in the clay galleries which can act as the potential binding sites for coordination of the titanium complex. Thus, the predried C30B reacted with toluene solution of Tp\(^{\text{Me}}\text{TCl}_3\) (1) for 24 h to generate the intercalated titanium catalyst 1/C30B (Scheme 1). The resulting metal content on the clay determined by ICP-OES was 20 µmol Ti g\(^{-1}\) of clay. On the basis of the powder X-ray diffraction (XRD) analysis, it was observed that the basal spacing of the predried C30B changes from 1.85 nm (2\(\theta\) = 4.8) to 2.18 nm (2\(\theta\) = 4.0) indicating that the intercalation of the titanium catalyst into the clay gallery took place (Figure 1). In this case, the increased spacing from predried C30B to 1/C30B is consistent with the increased intercalation of the clay gallery.

<table>
<thead>
<tr>
<th>Entry</th>
<th>T / °C</th>
<th>[Al]/[Ti]</th>
<th>time / min</th>
<th>(m_{\text{clay}}) / g</th>
<th>(m_{\text{PEclay}}) / g</th>
<th>activity(b)</th>
<th>(T_{c} / ^\circ\text{C})</th>
<th>(T_{m} / ^\circ\text{C})</th>
<th>(\Delta H / (mJ mg^{-1}))</th>
<th>(\chi / (%)</th>
<th>clay(^c) / (%)</th>
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<tbody>
<tr>
<td>1(d)</td>
<td>60</td>
<td>500</td>
<td>30</td>
<td>-</td>
<td>1.700</td>
<td>1739</td>
<td>119</td>
<td>136</td>
<td>200</td>
<td>70</td>
<td>-</td>
</tr>
<tr>
<td>2</td>
<td>30</td>
<td>500</td>
<td>60</td>
<td>0.103</td>
<td>0.183</td>
<td>40</td>
<td>113</td>
<td>136</td>
<td>117</td>
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<tr>
<td>3</td>
<td>60</td>
<td>500</td>
<td>60</td>
<td>0.100</td>
<td>0.700</td>
<td>300</td>
<td>116</td>
<td>136</td>
<td>166</td>
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<tr>
<td>4</td>
<td>80</td>
<td>500</td>
<td>60</td>
<td>0.105</td>
<td>0.499</td>
<td>197</td>
<td>113</td>
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<td>149</td>
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<tr>
<td>5(e)</td>
<td>60</td>
<td>2500</td>
<td>10</td>
<td>-</td>
<td>184.0</td>
<td>8762</td>
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<td>135</td>
<td>177</td>
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<td>126.0</td>
<td>6000</td>
<td>121</td>
<td>135</td>
<td>189</td>
<td>66</td>
<td>5</td>
</tr>
</tbody>
</table>

\(a\)Polymerization conditions: Fischer Porter bottle (100 mL), [Ti] = 2 µmol, toluene = 70 mL; MAO as cocatalyst. \(P_{\text{C2H4}} = 3.0\) atm; \(^b\)kg of PE/mol[Ti] h; \(^c\)percentage determined by TGA; \(^d\)ethylene polymerization using 1 in homogeneous phase. \([\text{Ti}] = 126 \mu\text{mol}, \text{hexane} = 2 \text{ L}; \text{MAO as cocatalyst,}\ P_{\text{C2H4}} = 6.0\) atm.
molecular dimensions of the titanium catalyst whereas the mesityl groups present in Tp³⁺ ligand determine significant steric crowding around the TiCl₃ unit.³⁴

The ethylene polymerization behavior of 1/C30B has been evaluated using methylaluminoxane (MAO) as cocatalyst. Representative results are given in Table 1. Initial study carried out at 60 °C with MAO-to-Ti ratio of 500 showed that this catalytic system was possible to polymerize ethylene with activity of 300 kg of PE per (mol [Ti] h) (entry 3). As expected, the intercalated catalyst showed lower activity than the one presented by the equivalent homogeneous system (entry 1, 1739 kg of PE per (mol [Ti] h)) in consequence of lower amount of potentially available Ti centers present into the clay gallery. However, lower ethylene diffusion into the gallery, which would induce catalyst decay, cannot be ruled out.

![Figure 1](image)

**Figure 1.** X-ray diffractograms of the activated C30B, 1/C30B and PE-C30BH nanocomposite.

The viscosity-average molecular weight (Mᵥ) values indicated the formation of ultra high molecular weight PE (UHMWPE); however the presence of clay particles provided a production of PE with lower molecular weight (2.94 × 10⁶ g mol⁻¹) in comparison with the neat PE (4.85 × 10⁶ g mol⁻¹). Such results suggest that the presence of well-dispersed clay in the PE matrix can retard the diffusion of ethylene and consequently the probability of chain propagation decreases with the clay loading.³⁸,³⁹

The montmorillonite exfoliation dispersion within the PE matrix has been analyzed by both XRD and transmission electronic microscopy (TEM). The powder XRD of the PE-C30BH showed the absence of the diffraction peak at 2Θ = 4.8 indicating the formation of an exfoliated PE-MMT nanocomposite (Figure 1). In addition, the appearance of weak intensity diffraction peak at 2Θ = 5.4 suggests the occurrence of non exfoliated clay with lower basal spacing (1.64 nm) that can be associated with the presence of natural no modified montmorillonite (MMT:Na).

Transmission electron micrographs of microtomed section of PE-C30BH nanocomposite confirmed homogeneous distribution of clay into the PE matrix as presented in Figure 2. Uniform dispersion is important because if the matrix consists of aggregates of particles, the stress field in the vicinity of the aggregate will be high, resulting in easier crack initiation and propagation, and consequent premature failure. In addition, Figure 2 reveals a good exfoliation of the C30B, with some few multilayer tactoids with expanded layer spacing still remaining.

Overall, their mechanical properties showed some improvements when compared with those ones displayed by the PE produced using exclusively 1. For instance, for the PE-C30BH it was observed an increase of the flexural modulus from 1050 (neat PE) to 1300 MPa, which is an improvement of 24%. Moreover, it was observed an increase of 10% in the temperature of deflection (HDT,
from 43 to 48 °C. From DMA results it can be found that the incorporation of C30B increases significantly the storage modulus (E’) of PE over the entire temperature range investigated which can be associated to the stiffening effect of the clay. In this case, the presence of C30B in the PE matrix increased storage modulus from 219.9 MPA (neat PE) to 853.9 Mpa as can be seen in Figure 3.

Conclusions

We have successfully intercalated 1 into the clay gallery and the resulting catalyst system was able to polymerize ethylene towards the production of PE-MMT nanocomposites. Both XRD and TEM results confirmed the uniform distribution of silicate layers of MMT in the whole PE matrix and the production of exfoliated PE-MMT nanocomposites. Some mechanical properties such as flexural modulus and storage modulus of PE-MMT nanocomposites showed some improvements when compared with those ones displayed by the neat PE produced using exclusively 1.

Acknowledgments

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